



流体输送模型(Pressure Changers)的分类

3

泵	Pump
压缩机	Compr
多级压缩机	MComper
阀门	Valve
管道	Pipe
管线	Pipeline

























Compr —计算模型①

◆Compr模块提供八种计算模型:
「标准等熵模型 Isentropic
ASME等熵模型 Isentropic using ASME method
GPSA等熵模型 Isentropic using GPSA method
ASME多变模型 Polytropic using ASME method
GPSA多变模型 Polytropic using GPSA method
分片积分多变模型 Polytropic using piecewise integration
正排量模型 Positive displacement
分片积分正排量模型 Positive displacement using piecewise integration

Compr —计算模型②	
◆八种计算模型如图:	
Compressor model Type: Isentropic Outlet spe Isentropic using ASME method Oitche Polytropic using GPSA method Polytropic Mechanical	

Compr —模型参数①

◆Compr模型有五种工作方式:

指定模型参数

●排出压力●压力增量●压力比率●所需功率

○特性曲线

Specifications Calculation	n Options Power Loss	Convergence	Integratio 🔺 🕨
Compressor model			
Type: Isentropic using /	\SME method	•	
Outlet specification			
 Discharge pressure: 	psi	-	
O Pressure change:	psi	-	
C Pressure ratio:			
O Brake horsepower:	hp	-	
O Use performance curves	to determine discharge co	nditions	
Efficiencies			
Isentropic:	olytropic: N	fechanical:	







▶多级多变压缩机(Multi-stage Polytropic Compressor)

▶多级正排量压缩机 (Multi-stage Positive Displacement

Compressor)

▶多级等熵压缩机(Multi-stage Isentropic Compressor)

MCompr —模型参数①

↔MCompr的模型参数有:

- ≻级数(Number of stages)
- 指定压缩机的级数

▶压缩机模型(Compressor model)

有六种计算模型供选用

>设定方式(Specification type)

指定压缩机的工作方式

←Configuration ← Material Heat-Work ← Specs ← Cooler Convergence
Number of stages:
Compressor model
C Isentropic C Polytropic using ASME method
👘 🔿 Isentropic using ASME method 🛛 🔿 Polytropic using GPSA method 👘 🔍
C Isentropic using GPSA method C Positive displacement
Specification type
🔹 🕞 Fix discharge pressure from last stage: 👘 🗸 🚽
O Fix discharge conditions from each stage
O Use performance curves to determine discharge conditions
Rating option

MCompr —模型参数2

MCompr的设定方式与Compr模块有所不同:

指定末级排出压力

(Fix discharge pressure from last stage)

指定每级排出条件

(Fix discharge conditions from each stage)

用特性曲线确定排出条件

(Use performance curves to determine discharge conditions)

Specification type:

O Fix discharge pressure from last stage:

 ps
1 · · · ·

Fix discharge conditions from each stage

O Use performance curves to determine discharge conditions





Multiple curves at different speeds

Number of curves:





↔阀门模型有三种应用方式:

▶绝热闪蒸到指定出口压力

Adiabatic flash for specified outlet pressure

▶对指定出口压力计算阀门流量系数

Calculate valve flow coefficient for specified outlet pressure

▶对指定阀门计算出口压力

Calculate outlet pressure for specified valve

Calculation type Adiabatic flash for specified outlet pressure (pressure changer) Calculate valve flow coefficient for specified outlet pressure (design) Calculate outlet pressure for specified valve (rating)





Valve —计算选项

- ◆计算阀门小开度状态时计算选项的设置很重要
 - 检查阻塞流动 (Check for choked flow)
 - 计算空泡系数 (Calculate cavitation index)
 - 设置最小出口压力等于阻塞压力
 - (Minimum outlet pressure:
 - Set equal to choked outlet pressure)





管道参数表	
长度 Pipe Parameters Thermal Specification Fittings Flash Options Length	
直径 Pipe length: ft ▼ Diameter Pipe schedules	
● diameter: ● Use pipe schedules ● Compute using user subroutine	
Elevation Options 121/12/12 ● Pipe rise: 0 ft Roughness: 0.00015 ft ● Pipe deg Erosional velocity 100	
angle: ' coefficient:	



Pipe —管件参数
◆连接方式:法兰连接/焊接Flanged/Welded,螺纹连接Screwed
◆管件数量: 闸阀Gate valves, 蝶阀Butterfly valves, 90度肘管Large 90 degree elbows, 直行三通 Straight tees, 旁路三通Branched tee
管件参数表单
连接方式 Connection type 管件数量 [©] Flanged welded Screwed 其余当量长度
Number of fittings Gate valves: Gate valves: Butterfly valves: Large 90 degrees elbows: Straight tees: Branched tees:
过程工程计算机应用基础





Pipeline — 管线参数②
在古NEW: <u> </u>
Pipeline — 管线参数③

单出如图管段数据(Segment data)对话框:

Segment No.	ə 1 🔽	Inlet node:	Outlet node:
Node parame	ters		
	Inlet node	Outlet	node
Fluid temp:		F	F 🔻
C-Erosion:	100	100	
		,	,
- Segment para	ameters		
Length:	ft	▼ Angle:	0 deg 💌
Diameter:	ft	✓ Annular OD:	ft 💌
		F#:-:	1

N≯

Close

例1】某离心泵以40m³/h的流量将贮水池中 ℃的热水用钢管输送到凉水塔顶,并经喷头喷 凉水池中以达到冷却的目的。已知水在进入喷头 前需要维持49kPa的表压强,喷头入口较离心泵 3m,离心泵较贮水池贮水池液面高5m。泵的吸 管长度(包括所有局部阻力的当量长度,下同) 60m,排出管长度为40m,二者的内径均为 0mm。试计算该离心泵所需提供的压头。

模拟实例

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搭建流程图:



指定单位制

※指定国际单位制,压力单位设为kPag,如图:

💽 Simulation 1 - Aspen Plus	V7.0 - aspenONE - [Setup Units-Se	ts US-1 - Data Browser]	
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Properties			
🚽 🖌 Flowsheet 🗸			

指定组分

·因离心泵输送的流体为水,所以只有一个组 分,如图:

🦲 Simulation 1 - Aspen Plus '	V7.0 - aspenONE - [Components Specifications - Data Browser]
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Components	
Specifications	
Assay/Blend	
🗄 🛅 Petro Character	
Attr-Comps	
UNIFAC Groups	
Comp-Groups	
🗄 🔂 Comp-Lists	Find Elec Wizard User Defined Reorder Review
🗄 🛅 Polymers	
Attr-Scaling	Component ID. If data are to be retrieved from databanks, enter either Component Name or



输入进料物流1的参数,如图:

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Properties	Temperature Mole-Frac V
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Results coefficient:	
EU Variables	
EO Input	
Spec Groups	
Ports	

表2某些工业管道的绝对粗糙度

45

金属管	绝对粗糙度(mm)	非金属管	绝对粗糙度(mm)
〔铜管、铜管及铝管	0.01-0.05	干净玻璃管	0.0015-0.01
E缝铜管或镀锌铁管	0.1-0.2	橡皮软管	0.01-0.03
新的铸铁管	0.25-1.0	木管道	0.25-1.25
新的无缝钢管	0.02-0.1	陶土排水管	0.45-6.0
		表面抹得较好的混凝土管	0.3-0.8
基腐蚀的无缝钢管	>0.5	表面平整的水泥管	0.3-0.8
旧的铸铁管	>0.85	新石棉水泥管	0.05-0.1
多年的煤气点管	0 5	中 等 状 况 的 石 棉 水 泥 管	0.03-0.8

指定管路参数(2) ⁴⁶ 指定管路B2的参数,包括长度、内径、位置抬高及粗糙 度,如图:

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	Ports		
	Stream Results		



指定泵的类型为Pump,排出压力为60 kPag,实际上泵的出口压力应该在物流4的压力指定后即可确定,但 Aspen为序贯模块法求解,所以需先输入一个初值,然后 再添加一个设计规定来准确计算该值,如图:

Simulation 1 - Aspen Plus V7.0 - aspenONE - [Block B3 (Pump) Setup - Data Browser] □ I file Edit View Data Tools Run Plot Library Window Costing Help □ D I File Add Real Real Real Real Real Real Real Real
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- Model
Blocks Pump outlet specification
B1 © Discharge pressure: 60 kPag -
C Pressure increase: N/sqm -
B3 C Pressure ratio:
C Power required: Watt
C Use performance C C Use performance curve to determine discharge conditions
Ser Subroun
Becute Efficiencies
Coversibles Pump: Driver:

添加设计规定(**1**)

在数据浏览器的Flowsheeting Options/Design Spec中新建一个设计规定,如图:

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Transfer		
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Model Analysis 1		
EO Configuration		

添加设计规定(**2**)

※点击上图的New,出现下图对话框,如图:

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For Help, press F1 C:\AspenTech\Aspen Plus V7.0 CAP Required Input Complete

添加设计规定(**3**)

点击上图的OK,出现下图窗口,如图:

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添加设计规定(4)

点击上图的New,出现下图对话框,并定义变量POUT, 如图:

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Balance 🚽
For Help, press F: C:\AspenTech\Aspen Plus V7.0 CAP Required Input Incomplete

添加设计规定(5)

点击上图的OK,出现下图对话框并对变量进行如下定义, 如图:

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Components Components Components Components Components Components Convergence	▼Variable Definition Select a variable category and reference Variable name: Variable name: Category C All C Blocks • Streams Model Utility • Physical Property Parameters • Reactions E0 input Open variable: Description:	Pe Reference Type: Stream-Var Substream: 4 Variable: PRES Units: kPag	Units-kPag

添加设计规定(**6**)

※调整离心泵的出口压力,使物流4的出口压力为 49kPag,如图:

💽 Simulation 1 - Aspen Plus V7.0 - aspenONE - [Design Spec DS-1 - Data Browser]
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DS-1
- C Varia
- 🥑 EO Input
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Stream Library Set point or target value for Spec expression. Constant, or Fortran expression in terms of

添加设计规定(**7**)

※调整离心泵的参数,如图:

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	Errors	0	0	0	
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					•
More					
All blocks have been execut	ted				
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查看模拟结果(1)

可见离心泵的压头为15.82m,流量为40m³/h如图:

🢽 Simulation 1 - Aspen Plus V7.0	- aspenONE - [Block B3	3 (Pump) Results - Data Browser]	
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例2】将IS80-65-125的离心泵放置在例1中给出 管路中,试计算该离心泵的实际功率,并确定该 的安装高度是否合适。

表1 IS80-65-125的特性曲线数据

Point	Flow	Head	Efficiency	NPSHR
1	30	22.5	0.64	3
2	50	20	0.75	3
3	60	18	0.74	3.5

隐藏设计规定(1)

·隐藏设计规定DS-1,如图:

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点击上图的Hide,出现下图对话框,如图:



隐藏设计规定(**3**)

点击上图的Yes,设计规定DS-1已被隐藏,如图:

💽 Simulation 1 - Aspen Plus	V7.0 - aspenONE - [Design Spec - Data Browser]
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For Help, press F1	C:\AspenTech\Aspen Plus V7.0 CAP Input Changed

由泵的特性曲线计算泵的出口状态

《将Pump outlet specification 内容由Discharge pressure更改为Use performance curve to determine discharge conditions,表示将由泵的特性曲线来计算泵 的出口状态,如图:

🥑 Simulation 1 - Aspen Plus	V7.0 - aspenONE - [Block B3 (Pump) - Data Browser]	_ [
💽 File Edit View Data	Tools Run Plot Library Window Costing Help	
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🖌 Components 📃 🔺	Specifications Calculation Options Flash Options Utility	
 Properties Flowsheet Streams Blocks B1 B2 B3 Secure Vser Subrout Block Option Results EO Variables EO Input Spec Groups Dest 	Model Pump Turbine Pump outlet specification Discharge pressure: Discharge pressure: Pressure ratio: Pressure ratio: Power required Valit Olde performance curve to determine discharge conditions Efficiencies Pump: Driver:	

在**Curve Setup**标签下指定特性曲线的形式, 如图:

	💽 Simulation 1 - Aspen Plus	V7.0 - aspenONE - [Block B3 (Pump) Performance Curves - Data Browser]
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l	🍼 Performance Curves 💌 🖻	
I	🖌 Components 📃	VCurve Setup VCurve Data VEfficiencies VNPSHR Operating Specs)
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I	Streams	
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I	⊟ <u>B</u> 3	· Single curve at operating speed 主 二收益 〉 撮 化 杜
I	🗸 🍼 Setup	C Single curve at reference speed 不不你们人保存我
I	🧭 🝼 Performance	│ [○] Multiple curves at different speeds
I	🛛 🍼 User Subrout	
I		
I	Results	Uptions
	EO Variables	
	🥑 EO Input	
	🛛 🍼 Spec Groups	
	Ports	
	Stream Resul	
	Custom Strea	Curve is input as tabular data. The table is interpolated at runtime.
	🛛 Utilities 🛛 👻	

指定离心泵特性曲线参数(1)

在Curve Data标签下输入压 头流量数据,如图:

💽 Simulation 1 - Aspen Plus V	7.0 - aspenONE - [Block B3 (Pump) Performance Curves - Data Browser]
💽 File Edit View Data	iools Run Plot Library Window Costing Help
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Components	✓Curve Setup ✓Curve Data ✓Efficiencies ✓NPSHR Operating Specs
Properties Flowsheet Streams	Units of curve variables Head: meter - Flow. cum/hr -
Blocks ⊕ ☆ B1 ⊕ ☆ B2	Curve speeds Curve No.: 1 Shaft Speed No. Shaft Speed Hz
=-⊡ B3 ✓ Setup	1 22.5 30 **
- 🧭 Performance	2 20 50
User Subrout	3 18 60
Block Option	4 21 40
Results	*
EO Variables	
EO Input	
Spec Groups	
Ports	

指定离心泵特性曲线参数(2) ⁶⁴ 在Efficiencies标签下输入效 率流量数据,如图:

C Simulation 1 - Aspen Plus V7.0 - aspenONE - [Block B3 (Pump) Performance Curves - Data Browser]
🔝 File Edit View Data Tools Run Plot Library Window Costing Help
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Ø Performance Curves ▼ ■ ■ ✓ All ▼ >> □ × × □ × □ × □ × □ × □ × □ × □ × □ × □
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Properties
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Streams Efficiency: Fraction Flow:
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B1 Curve Speeds
T → B2
B3 Point Efficiency Flow
Setup
2 0.75 50
4 Her Subraut 3 074 60
EO Input
Spec Groups
Ports
Stream Resul

指定离心泵特性曲线参数(3)

※在NPSHR标签下输入必须汽 蚀余量流量数据,如图:

🥑 Simulation 1 - Aspen Plus V7.0 - aspenONE - [Block B3 (Pump) Performance Curves - Data Browser] 📃 🔲	×
🔝 File Edit View Data Tools Run Plot Library Window Costing Help	×
🕑 Performance Curves 🔹 🗈 😰 US-1 🔹 🗲 🄶 < All 🔹 >> 🗌 🕲 🗐 🕪 🖄 🖉 🗡	
<u> </u>	
Properties Units of curve variables Flowsheet NPSH required: meter Streams Flow: curv/hr Blocks Flow: curv/hr	
B1 NPSH-required vs. flow table Curve speeds Curve No.: Curve No.: Curve Shaft speed No.	
V Setup	
V Performance 1 3 30	
User Subrout 2 3 50	
Block Option 3 3.5 60	
Det al lot	
∑ Stream Result	



Simulation 1 - Aspen Plus V7.0 - aspenONE - [Control Panel] File Edit View Data Tools Run Library Window Costing Help File Edit View Data Tools Run Library Window Costing Help File Edit View Data Tools Run Library Window Costing Help File Edit View Data Tools Run Library Window Costing Help File Edit View Data Tools Run Library Window Costing Help File Edit View Data Tools Run Library Window Costing Help File Edit View Data Tools Run Library Window Costing Help File Edit View Data Tools Run Library Window Costing Help File Edit View Data Tools Run Library Window Costing Help File Edit View Data Tools Run Library Window Costing Help File Edit View Data Tools Run Library Window Costing Help File Edit View Data Tools Run Library Window Costing Help File Edit View Data Tools Run Library Window Costing Help File Edit View Data Tools Run Repute Run Repute Run Repute Run Repute Value Solve For Forst IIVE SUCTION HEAD IS LESS THAN REQUIRED VALUE ->Simulation calculations completed **** Summary of Errors **** Physical Property System Simulation Terminal Errors 0 0 Warnings 0 0 Warnings 0 0	Simulation 1 - Aspen Plus File Edit View Data	V7.0 - aspenONE - Tools Run Libra	[Control Panel]			<u>_ 🗆 X</u>
File Edit View Data Tools Run Library Window Costing Help Image: Solve	File Edit View Data	Tools Run Libra	MAC allowed			
Image: Solve Image: Solve <td< th=""><th></th><th></th><th>ary window</th><th>Costing Help</th><th></th><th>_ 8 ×</th></td<>			ary window	Costing Help		_ 8 ×
Solve Solve Calculation Sequen ->Generating block results B1 B3 B2 ->Generating block results B10ck: B3 Model: FUMP * WARNING NET POSITIVE SUCTION HEAD IS LESS THAN REQUIRED VALUE ->Simulation calculations completed **** Summary of Errors *** Physical Property System Severe Errors 0 0 0 Errors 0 Warnings 0		8 🕺 🖬 🖌 😫	\$ 🛱 🝕 💞	▶ 🔢 🕨 🕨	H 🔳 🔣 🗹 🛛	3 💽 🔍 🔍 🔤
Calculation Sequen Solve Secretaring block results B1 B3 B2 Simulation calculations completed **** Summary of Errors *** Physical Property System Simulation Terminal Errors 0	▲▲ ▲ छ र छर छ	8				
Calculation Sequen B1 B3 B2 ->Generating block results Block: B3 Model: FUMP * WARNING NET POSITIVE SUCTION HEAD IS LESS THAN REQUIRED VALUE ->Simulation calculations completed **** Summary of Errors *** Physical Property System Simulation Terminal Errors 0 0 0 Severe Errors 0 0 0 Errors 0 0 0 Warnings 0 0 6				= <i>#</i> -		
Calculation Sequen B1 B1 B2 B1 K KARNING NET POSITIVE SUCTION HEAD IS LESS THAN REQUIRED VALUE ->Simulation calculations completed **** Summary of Errors *** Physical Property System Simulation Terminal Errors 0 0 0 CErrors				= // .		
B1 B3 B3 B2 B2 B2 B1 B2 B1 B3 B1 B1 B3 B1 B1 B3 B1 B1 B3 B1 B1 B3 B1 B1 B3 B1 B1 B3 B1 B1 B3 Model: FUMP * WARNING NET POSITIVE SUCTION HEAD IS LESS THAN REQUIRED VALUE ->Simulation calculations completed **** Summary of Errors *** Physical Property System Simulation Terminal Errors 0 0 0 Severe Errors 0 0 0 Errors 0 0 0 Warnings 0 0 6	Calculation Sequen					<u> </u>
B3 B2 B2 B2 B2 B2 B3 B10ck: B3 Model: FUMP * WARNING NET POSITIVE SUCTION HEAD IS LESS THAN REQUIRED VALUE ->Simulation calculations completed **** Summary of Errors *** Physical Property System Simulation Terminal Errors 0 0 0 Severe Errors 0 0 0 Warnings 0 0 6	B1	Senerating block	results			
B2 * WARNING NET POSITIVE SUCTION HEAD IS LESS THAN REQUIRED VALUE ->Simulation calculations completed *** Summary of Errors *** Physical Property System Simulation Terminal Errors 0 0 0 Severe Errors 0 0 0 Errors 0 0 0 Warnings 0 0 6	🛅 B3	Block: B3	Model: PUMP))		
NET POSITIVE SUCTION HEAD IS LESS THAN REQUIRED VALUE ->Simulation calculations completed *** Summary of Errors *** Physical Property System Simulation Terminal Errors 0 0 0 Severe Errors 0 0 0 Errors 0 0 6	B2	* WARNING				
->Simulation calculations completed *** Summary of Errors *** Physical Property System Simulation Terminal Errors 0 0 0 Severe Errors 0 0 0 Errors 0 0 0 Warnings 0 0 6		NET POSITIVE	SUCTION HEAD) IS LESS THAN R	EQUIRED VALUE	
->Simulation calculations completed *** Summary of Errors *** Physical Property System Simulation Terminal Errors 0 0 0 Severe Errors 0 0 0 Errors 0 0 0 Warnings 0 0 6						
*** Summary of Errors *** Physical Property System Simulation Terminal Errors 0 0 0 Severe Errors 0 0 0 Errors 0 0 0 Warnings 0 0 6		>Simulation calcu	lations compl	eted		
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*** Summary of Errors *** Physical Property System Simulation Terminal Errors 0 0 0 Severe Errors 0 0 0 Errors 0 0 0 Warnings 0 0 6						
Physical Property System Simulation Terminal Errors 0 0 0 Severe Errors 0 0 0 Errors 0 0 0 Warnings 0 0 6			***	Summary of Erro	rs ***	
Property System Simulation Terminal Errors 0 0 0 Severe Errors 0 0 0 Errors 0 0 0 Warnings 0 0 6			Physical			
Terminal Errors 0 0 0 Severe Errors 0 0 0 Errors 0 0 0 Warnings 0 0 6			Property	System	Simulation	
Severe Errors 0 0 0 Errors 0 0 0 Warnings 0 0 6		Terminal Errors	0	0	0	
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warnings U U O		Errors	0	0	0	
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Nores	More 😻					
All blocks have been executed	All blocks have been execute	ed				
	Simulation ru	C:\	AspenTech\Asp	en Plus V7.0 CAP	Results Ava	ilable with Warnings //



模拟运行之后有警告,查看迭代信息,发现警告信息含 义为汽蚀余量小于必须汽蚀余量,如图:产生该信息 的原因是泵的安装高度过大,必须降低安装高度。

🕐 Simulation 1 - Aspen Plus V7.0 - aspenONE - [Control Panel]	×
🔝 File Edit View Data Tools Run Library Window Costing Help 📃 🖪	PX
Dei si	
▶ ▷ K ■ Solve ▼ 🕱 🗹	
⊡ 🗎 Calculation Sequen	
->Generating block results	
BIOCK: B3 MODEL: PUMP	
NET POSITIVE SUCTION HEAD IS LESS THAN REQUIRED VALUE	
· · · · · · · · · · · · · · · · · · ·	
- Simulation Calculations completed	
*** Summary of Errors ***	
Physical	
Property System Simulation	
Terminal Errors 0 0 0	
Severe Errors 0 0 0	
Errors 0 0 0	
warnings 0 0 6	
	-
	•

降低安装高度(1)

将B1的高度改为3m,即泵的安装高度 由5m降低至3m,如图:

🥑 Simulation 1 - Aspen Plus V	7.0 - aspenONE - [Block B1 (Pipe) - Data Browser]
🔝 File Edit View Data T	ools Run Plot Library Window Costing Help
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🔁 B1 🗨 🖻	😫 US-1 🔹 🗲 🔿 < (Al 🔹 🏹 🛄 🚳 🔊 🕨 🖄 🗡
🕀 🗹 Setup	✓Pipe Parameters Thermal Specification Fittings1 Fittings2 Flash Options
 ⊕	Length Pipe length: 60 meter 💌
E∰ Streams E∰ Blocks	Diameter Pipe schedules Inner 100 diameter Material:
∛ Setup ∛ Advanc	C Use pipe schedules C Compute using user subroutine
User Su	Elevation Options
Dynami	Pipe rise Pipe rise Roughness: 0.25 mm
Biock C	C Pipe rad V Erosional velocity 100
EO Var	
EO Inpi	
Spec G	
Ports	
Stream	
E Custom E B2 ▼	ets you type the change in pipe elevation from pipe entrance to exit. Flow is uphill if positive, downhill if negative.
For Help, pre	C:\AspenTech\Aspen Plus V7.0 CAP Results Available with Warnings

降低安装高度(2)

※将B2的高度改为5m,如图:

🥑 Simulation 1 - /	Aspen Plus \	7.0 - aspenONE - [Block B2 (Pipe) - Data Browser]
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	a 🖻 🖻	N II - A S S A A A A A A A A A A A A A A A A
🔁 B2	- 🗈	🖹 US-1 🔹 🗲 🔿 < 🗛 🔹 💌 💶 💌 💭 🔛
	EO Var 📥	✓Pipe Parameters Thermal Specification Fittings1 Fittings2 Flash Options
	EO Inpi Spec G Ports	Length Pipe length: 40 meter 💌
<mark>∆</mark> <mark>∆</mark> 62	Stream Custom	Diameter Pipe schedules C Inner 100 mm Material:
	Setup Advanc	C Use pipe schedules Schedule:
- V	User Su	Elevation
	Dynami	Pipe rise: meter Roughness: 0.25 mm m
	Block C	C Pipe rad v Erosional velocity 100
	FO Var	
	EO Inp	
	Spec G	
	Ports	
	Stream	
	Custom	Lets you type the change in pipe elevation from pipe entrance to exit. Flow is uphill if



说明3m的安装高度是合适的,如图:

Simulation 1 - Aspen Plus V7.0 - aspenONE -	[Control Pane	Ŋ		_ 🗆 🗙
💽 File Edit View Data Tools Run Libra	ary Window	Costing Help		_ 8 ×
D # 8 &6 % <mark>74</mark>	\$ 5 € 60	▶ 🗉 ▶	D K 🔳 🔣 🗹 🧧	
Solve III	1	≣%▼		
Calculation Sequen UNLESS NPHAS	E=1 IS SPECT	IFIED.		▲
B1 CALCULATIONS	WILL CONTIN	NUE WITH NPHAS	E=1, PHASE=LIQUID	
- B3				
B2 ->Generating block	results			
Block: B3	Model: PUN	1P		
Simulation colour	lationa com	lotod		
->Simulation calcu	Tacions com	pieced		
	***	Summary of E	rrors ***	
	Physical			
	Property	System	Simulation	
Terminal Errors	0	0	0	
Severe Errors	0	0	0	
Errors	0	0	0	
warnings	U	0	0	
				_
More				
All blocks have been executed				

查看泵的计算结果

泵的计算结果已列入表中,如图:

🢽 Simulation 1 - Aspen Plus	V7.0 - aspenONE - [Block B3 (Pump) Results - Data Browser]
🔝 File Edit View Data	Tools Run Plot Library Window Costing Help
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🔽 Results 💽 🖻	
Components	Summary Balance Performance Curve Utility Usage
	Pump results 有效功率
🗄 🚮 Streams	Fluid power: 2243.62193 Watt 主 轴功率
🖻 🔂 Blocks	Brake power: 3205.15438 Watt 自机功率
🕂 🕀 🔂 🛃	Electricity: 3205.15438 Watt
Ē <mark>™</mark> B2	Volumetric flow rate: 40.0007966 cum/hr 体积流量
⊟ <mark>≣∕</mark> B3	Pressure change: 201921.953 N/sqm IF 力美
🧹 Setup	NPSH available: 37.0960373 J/kg
🛛 🍼 🗸 Perforn	│ NF5H requi <mark>坐头 29.4199505</mark> J/kg _
🚽 🗸 User Sı	He ad developed: 20.9999047 meter
	Punper Mar Punper August 20.70000433
Results	Net work required 3205.15438 Watt
EO Var	
🚽 🗸 🗸 EO Inpi	
🚽 🍼 🍼 Spec G	
Ports	
Chursens	

72) 【例3】流量为 5000 kg/h, 压强为 7 ar的饱和水蒸汽流经 \$108×4mm 的管 f。管道长 20 m, 出口比进口高 5 m, 【糙度为 0.05 mm。管道采用法兰连接, ·装有闸阀1个,90° 肘管2个。环境 L度为 20°C, 传热系数为 20 W/(m²·K)。 **:** 出口处蒸汽的压强、温度和含水率,

模拟实例
模拟实例

- 例4】流量为 100 m³/h, 温度为 50 °C, 压 为 5 bar的水流经 φ108×4 的管线。管线首 向东延伸 5 m, 再向北 5 m, 再向东 10 m, 向南 5 m, 然后升高 10 m, 再向东 5 m。 内壁粗糙度为 0.05 mm。



